

## Solubilities of 1-Hexyl-3-methylimidazole Nitrate and 1-Octyl-3-methylimidazole Nitrate in Selected Solvents

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**ABSTRACT:** Solubilities of two ionic liquids, 1-hexyl-3-methylimidazolium nitrate ([HMIM][NO<sub>3</sub>]) and 1-octyl-3-methylimidazolium nitrate ([OMIM][NO<sub>3</sub>]), in 10 organic solvents (*n*-pentane, *n*-hexane, cyclohexane, *n*-heptane, *n*-octane, benzene, toluene, *o*-xylene, *p*-xylene, and *m*-xylene) were measured in the range between (278.15 and 343.15) K using a static analytical gravimetric method, respectively. The logarithm of the mole fraction solubilities of these two ILs in the 10 selected solvents was correlated by a linear function of inversed temperatures.

### INTRODUCTION

Ionic liquids (ILs) have been studied widely in many branches of chemistry these years<sup>1</sup> because of their interesting physical and chemical properties. They can be used as solvents for new syntheses<sup>2</sup> and electrolytes in electrochemical devices.<sup>3–6</sup> This is mainly due to many of their fascinating properties, such as high thermal and chemical stability at high temperatures, negligible vapor pressure, nonflammability, and high loading capacity. The properties of the ILs can be adjusted by altering the cation or anion, the chain length of the alkyl rests, and the substituent, so ILs are also known as “designer solvents”.<sup>7</sup>

1-Hexyl-3-methylimidazolium nitrate ([HMIM][NO<sub>3</sub>]) (CAS Registry No. 203389-26-8) and 1-octyl-3-methylimidazolium nitrate ([OMIM][NO<sub>3</sub>]) (CAS Registry No. 203389-27-9) are two halogen-free ILs and thus more environmentally friendly than the halogenated ones.<sup>8</sup> The physicochemical information of ILs either in pure forms or as binaries with organic or inorganic compounds is of importance for their industrial application. The study on their phase behavior with organic solutes is of interest. In view of the industrial importance of phase equilibria involving ILs such as vapor–liquid equilibria, liquid–liquid equilibria, and solid–liquid equilibria, the solubilities of a number of ionic liquid in different solvents have been investigated, for example, 1-ethyl-3-methylimidazolium hexafluorophosphate ([emim][PF<sub>6</sub>]),<sup>9</sup> 1-ethylpyridinium hexafluorophosphate ([EPy][PF<sub>6</sub>]),<sup>10</sup> and didecylmethylammonium nitrate ([DDA][NO<sub>3</sub>]).<sup>11</sup> However, solubility data of [OMIM][NO<sub>3</sub>] and [HMIM][NO<sub>3</sub>] are not found in literature.

In this study, solubilities of two ILs, [HMIM][NO<sub>3</sub>] and [OMIM][NO<sub>3</sub>], in 10 selected solvents (*n*-pentane, *n*-hexane, cyclohexane, *n*-heptane, *n*-octane, benzene, toluene, *o*-xylene, *p*-xylene, and *m*-xylene) are measured.

### EXPERIMENTAL SECTION

**Materials.** 1-Hexyl-3-methylimidazolium nitrate (99.5 %) and 1-octyl-3-methylimidazolium nitrate (99.5 %) were purchased from the Shanghai Chengjie Chemical Reagents Company. The chemical shifts for the <sup>1</sup>H NMR spectrum (parts per million, C<sub>3</sub>D<sub>6</sub>O) appeared as follows: [HMIM][NO<sub>3</sub>], δ: 9.07

(s, 1H, CH–N), 7.73–7.66 (d, 2H, CH=CH–N), 4.16–4.12 (t, 2H, CH<sub>2</sub>Me), 3.84 (s, 3H, CH<sub>3</sub>N), 1.79–1.74 (t, 2H, CH<sub>2</sub>N), 1.26–1.22 (m, 6H, (CH<sub>2</sub>)<sub>3</sub>), 0.87–0.84 (t, 3H, CH<sub>2</sub>CH<sub>3</sub>); [OMIM][NO<sub>3</sub>], δ: 9.07 (s, 1H, CH–N), 7.74–7.67 (d, 2H, CH=CH–N), 4.15–4.12 (t, 2H, CH<sub>2</sub>Me), 3.84 (s, 3H, CH<sub>3</sub>N), 1.80–1.76 (t, 2H, CH<sub>2</sub>N), 1.26–1.23 (m, 10H, (CH<sub>2</sub>)<sub>5</sub>), 0.86–0.84 (t, 3H, CH<sub>2</sub>CH<sub>3</sub>). All of the solvents in the measurement were purchased from different chemical reagent producers as listed in Table 1. Their mass fraction purities are as follows: *n*-pentane (0.990), *n*-hexane (0.990), cyclohexane (0.995), *n*-heptane (0.985), *n*-octane (0.990), benzene (0.995), toluene (0.995), *o*-xylene (0.985), *p*-xylene (0.950), and *m*-xylene (0.950). The water content in each solvent was less than 0.20 %. All the reagents in this work were analytical reagent (AR) grade and used without further purification.

**Apparatus.** A jacketed equilibrium cell with a working volume of 100 mL was immersed in a circulating water bath with a thermostat (type 50 L, Shanghai Laboratory Instrument Works Co. Ltd.) with a precision of ± 0.05 K as described by Shang et al.<sup>12</sup> An analytical balance (type TG328B, Shanghai Balance Instrument Works Co.) with an uncertainty of ± 0.1 mg, a magnetic stirrer, and a calibrated thermometer with a precision of 0.1 K were used in the experiment. The equilibrium cell was sealed to prevent the evaporation of solvent or solute during the experiment.

**Solubility Measurement.** The solubilities were measured by a gravimetric method.<sup>13</sup> For each measurement, an excess mass of IL was added to a known mass of solvent. Then the equilibrium cell was heated to a constant temperature with continuous stirring. After at least 1 h (once the temperature of water bath approached a constant value, the actual value of temperature was recorded), the stirring was stopped, and the solution was kept still until it was clear and the excess mass of IL was in the lower portion. About 2 mL of the clear upper portion of the solution

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Table 1. Boiling Points of the Solvents Used in This Work

solvent	boiling point/K	producers	mass of residue after evaporation/%
<i>n</i> -pentane	309.25	<sup>d</sup>	0.050
<i>n</i> -hexane	342.15	<sup>a</sup>	0.001
cyclohexane	353.89	<sup>b</sup>	0.002
<i>n</i> -heptane	371.55	<sup>a</sup>	0.002
<i>n</i> -octane	398.15	<sup>a</sup>	0.002
benzene	353.25	<sup>b</sup>	0.001
toluene	383.75	<sup>b</sup>	0.001
<i>o</i> -xylene	417.15	<sup>c</sup>	0.005
<i>m</i> -xylene	412.45	<sup>c</sup>	0.005
<i>p</i> -xylene	411.15	<sup>c</sup>	0.005

<sup>a</sup> Tianjin Fuchen Chemical Reagent Co., Ltd. <sup>b</sup> Beijing Chemical Works.

<sup>c</sup> Sinopharm Chemical Reagent Co., Ltd. <sup>d</sup> Acros Organics (Geel, Belgium).

was withdrawn to another previously weighed measuring vial ( $m_0$ ) with a preheated on-off injector. The vial was quickly and tightly closed and weighed ( $m_1$ ) to determine the mass of the sample ( $m_1 - m_0$ ). The vial was uncovered and then covered with a piece of filter paper to prevent dust contamination. After the solvent in the vial had completely evaporated, the vial was dried and reweighed ( $m_2$ ) to determine the mass of the residue IL ( $m_2 - m_0$ ). The IL concentration of the sample solution in mole fraction,  $x$ , is determined from eq 1

$$x = \frac{(m_2 - m_0)/M_1}{(m_2 - m_0)/M_1 + (m_1 - m_0)/M_2} \quad (1)$$

where  $M_1$  and  $M_2$  are the molar mass of the IL and solvent, respectively.

A different dissolution time was tested to determine a suitable equilibrium time. It was found that 1 h was enough for [OMIM][NO<sub>3</sub>] and [HMIM][NO<sub>3</sub>] to reach equilibrium in the solvent. Three parallel measurements were performed at the same composition of solvent at each temperature, and an average value was given. The maximum relative deviation of each triplicate data is 0.25 %, and the minimum is 0.15 %. The estimated relative uncertainty of the solubility values based on error analysis and repeated observations is within 2 %. The uncertainty in the experimental solubility is due to uncertainties in the temperature measurement, weighing procedure, and instabilities of the water bath. The temperature range for the solubility measurement in different organic solvents should be below the boiling point of the respective solvent. The evaporation temperatures of the solvents used in this work are listed in Table 1.

## RESULTS AND DISCUSSION

Solubilities of [HMIM][NO<sub>3</sub>] and [OMIM][NO<sub>3</sub>] in 10 selected organic solvents were measured in the range between (278.15 and 343.15) K. The mole fraction solubility data of these two ILs at different temperatures are presented in Table 2.

**Correlation.** Since in the temperature range studied the molar enthalpy of IL solutions can be considered temperature-independent, the experimental solubility data can be correlated by the following equation:<sup>14–16</sup>

$$\ln x = A + B/(T/K) \quad (2)$$

Table 2. Mole Fraction Solubilities ( $x$ ) of ILs in Pure Organic Solvents at Different Temperatures

ILs	solvent	T/K	10 <sup>3</sup> $x$	( $x - x^{\text{calcd}}$ )/ $x$
[HMIM][NO <sub>3</sub> ]	<i>n</i> -pentane	278.15	0.359	−0.0005
		283.15	0.397	−0.0042
		288.15	0.442	0.0056
		293.15	0.484	−0.0011
		298.15	0.534	0.0053
		303.15	0.578	−0.0051
		308.15	0.629	−0.0006
		313.15	0.683	0.0014
		318.15	0.739	−0.0244
	<i>n</i> -hexane	288.15	0.306	−0.0006
		293.15	0.362	0.0014
		298.15	0.420	−0.0244
		303.15	0.492	−0.0062
		308.15	0.575	0.0090
		313.15	0.693	0.0264
		318.15	0.794	0.0211
		323.15	0.895	−0.0003
		328.15	0.995	−0.0064
	cyclohexane	293.15	0.304	0.0106
		298.15	0.357	0.0251
		303.15	0.400	−0.0002
		308.15	0.446	−0.0277
		313.15	0.516	−0.0118
		318.15	0.592	−0.0025
		323.15	0.674	0.0044
		328.15	0.751	−0.0079
		333.15	0.857	0.0092
	<i>n</i> -heptane	338.15	0.970	0.0199
		313.15	0.268	0.0046
		318.15	0.358	−0.0099
		323.15	0.490	0.0010
		328.15	0.629	0.0081
		333.15	0.841	−0.0035
338.15		1.093	−0.0002	
343.15		1.419	−0.0001	
<i>n</i> -octane		293.15	0.203	−0.0142
	298.15	0.234	−0.0089	
	303.15	0.268	0.0138	
	308.15	0.299	0.0101	
	313.15	0.344	0.0153	
	318.15	0.380	0.0038	
	323.15	0.421	−0.0072	
	328.15	0.458	−0.0133	
	333.15	0.518	0.0004	
benzene	338.15	0.568	−0.0091	
	343.15	0.631	−0.0010	
	298.15	0.219	−0.0059	
	303.15	0.263	−0.0006	
	308.15	0.308	−0.0100	
	313.15	0.382	0.0044	
	318.15	0.454	0.0087	
	323.15	0.536	0.0058	
	328.15	0.610	0.0014	
333.15	0.714	−0.0099		
338.15	0.832	0.0018		
343.15	0.962	0.0032		

Table 2. Continued

ILs	solvent	T/K	$10^3x$	$(x - x^{\text{calcd}})/x$	
[OMIM][NO <sub>3</sub> ]	toluene	298.15	0.278	0.0040	
		303.15	0.334	0.0006	
		308.15	0.390	-0.0141	
		313.15	0.482	-0.0037	
		318.15	0.585	0.0214	
		323.15	0.686	0.0111	
		328.15	0.776	0.0006	
		333.15	0.904	-0.0162	
		338.15	1.061	-0.0023	
		343.15	1.227	0.0034	
		o-xylene	298.15	1.332	-0.0156
			303.15	1.450	-0.0110
	308.15		1.599	0.0082	
	313.15		1.732	0.0127	
	318.15		1.866	0.0136	
	323.15		1.983	0.0038	
	328.15		2.133	0.0075	
	333.15		2.266	0.0014	
	338.15		2.400	-0.0062	
	343.15		2.533	-0.0151	
	m-xylene		298.15	2.392	-0.0055
			303.15	2.715	0.0049
		308.15	3.032	0.0028	
		313.15	3.368	-0.0011	
		318.15	3.764	0.0046	
		323.15	4.127	-0.0058	
		328.15	4.578	-0.0010	
		333.15	5.051	0.0011	
		338.15	5.534	-0.0009	
		343.15	6.070	0.0010	
		p-xylene	298.15	0.795	-0.0178
			303.15	0.896	-0.0127
	308.15		1.024	0.0091	
313.15	1.140		0.0085		
318.15	1.277		0.0168		
323.15	1.409		0.0138		
328.15	1.550		0.0109		
333.15	1.686		-0.0001		
338.15	1.823		-0.0149		
343.15	1.995		-0.0144		
n-pentane	278.15		0.687	-0.0029	
	283.15		0.816	0.0053	
	288.15	0.955	0.0042		
	293.15	1.103	-0.0035		
	298.15	1.266	-0.0131		
	303.15	1.493	0.0098		
	n-hexane	288.15	0.683	0.0160	
		293.15	0.780	-0.0283	
		298.15	0.919	-0.0091	
		303.15	1.129	0.0120	
		308.15	1.282	-0.0096	
		313.15	1.624	0.0190	
318.15		1.844	0.0273		
323.15		2.056	-0.0121		
328.15		2.316	-0.0119		
333.15		2.706	-0.0046		

Table 2. Continued

ILs	solvent	T/K	$10^3x$	$(x - x^{\text{calcd}})/x$	
[OMIM][NO <sub>3</sub> ]	cyclohexane	293.15	0.775	-0.0014	
		298.15	0.901	-0.0225	
		303.15	1.056	-0.0036	
		308.15	1.244	0.0197	
		313.15	1.462	0.0131	
		318.15	1.685	0.0149	
		323.15	1.909	-0.0003	
		328.15	2.121	-0.0072	
		333.15	2.440	-0.0072	
		338.15	2.754	-0.0061	
		n-heptane	293.15	0.342	0.0247
			298.15	0.407	-0.0115
303.15	0.488		-0.0082		
308.15	0.586		-0.0009		
313.15	0.728		0.0039		
318.15	0.856		-0.0102		
323.15	1.010		-0.0224		
328.15	1.188		-0.0013		
333.15	1.427		0.0112		
338.15	1.664		0.0084		
n-octane	343.15		1.932	0.0055	
	293.15		0.355	0.0377	
	298.15	0.411	-0.0157		
	303.15	0.502	-0.0096		
	308.15	0.605	-0.0106		
	313.15	0.733	-0.0002		
	318.15	0.866	-0.0095		
	323.15	1.009	-0.0275		
	328.15	1.230	0.0057		
	333.15	1.455	0.0133		
	benzene	338.15	1.681	0.0021	
		343.15	1.976	0.0127	
298.15		0.303	-0.0002		
303.15		0.357	0.0046		
308.15		0.410	-0.0045		
313.15		0.490	-0.0047		
318.15		0.572	0.0031		
323.15		0.661	-0.0019		
328.15		0.751	0.0078		
333.15		0.860	-0.0042		
toluene		338.15	0.981	-0.0001	
		343.15	1.114	-0.0001	
	298.15	0.371	0.0111		
	303.15	0.430	-0.0074		
	308.15	0.500	-0.0026		
	313.15	0.598	0.0016		
	318.15	0.699	0.0135		
	323.15	0.806	0.0098		
	328.15	0.892	-0.0044		
	333.15	1.025	-0.0106		
	338.15	1.173	0.0016		
	o-xylene	343.15	1.329	-0.0021	
298.15		4.998	-0.0048		
303.15		5.290	-0.0010		
308.15		5.581	0.0013		

Table 2. Continued

ILs	solvent	T/K	10 <sup>3</sup> x	(x - x <sup>calcd</sup> )/x
		313.15	5.873	0.0026
		318.15	6.164	0.0030
		323.15	6.456	0.0027
		328.15	6.747	0.0017
		333.15	7.039	0.0002
		338.15	7.330	-0.0017
		343.15	7.622	-0.0040
	<i>m</i> -xylene	298.15	5.256	-0.0102
		303.15	5.655	-0.0022
		308.15	6.054	0.0029
		313.15	6.453	0.0056
		318.15	6.852	0.0063
		323.15	7.251	0.0056
		328.15	7.650	0.0035
		333.15	8.049	0.0004
		338.15	8.448	-0.0036
		343.15	8.847	-0.0083
	<i>p</i> -xylene	298.15	3.076	-0.0103
		303.15	3.310	-0.0058
		308.15	3.576	0.0046
		313.15	3.826	0.0076
		318.15	4.076	0.0083
		323.15	4.309	0.0035
		328.15	4.576	0.0047
		333.15	4.826	0.0008
		338.15	5.076	-0.0040
		343.15	5.326	-0.0097

where *A* and *B* are correlation parameters for each solvent. The correlation constants obtained from the fitting of IL solubility data are listed in Table 3. The relative standard deviations (RSDs) for each solvent, defined by eq 3, are also presented in Table 3.

$$\text{RSD} = \left[ \frac{1}{N} \sum_{i=1}^n \left( \frac{x_i - x_i^{\text{calcd}}}{x_i} \right)^2 \right]^{1/2} \quad (3)$$

where superscript calcd stands for the calculated values and *N* is the number of experimental points. The plots of ln *x* versus 1/*T* of two ILs are shown in Figures 1 and 2, respectively. From these figures it can be seen that, within the temperature range of the measurements, the ILs [HMIM][NO<sub>3</sub>] and [OMIM][NO<sub>3</sub>] are partially soluble in the nonpolar or weak-polar solvents studied and their solubilities in the selected solvents increase with temperature. The logarithm of mole fraction solubilities of these two ILs in the 10 selected solvents were correlated by a linear function of inversed temperatures, and the solubilities calculated from the correlation are in good agreement with the experimental data.

For the straight-chain alkanes, the mole fraction solubilities of these two ILs are ranked as *n*-pentane > *n*-hexane > *n*-heptane > *n*-octane, which may result from the difference in their molecular mass. For the three aromatic solvents investigated, the mole fraction solubilities of these two ILs are ranked as xylene > methylbenzene > benzene, which were consistent with their

Table 3. Parameters of Equation 2 and Relative Standard Deviations (RSDs) of the Measured Solubility of Solutes in Selected Solvents from the Calculated Results

ILs	solvent	A	B	RSD
[HMIM][NO <sub>3</sub> ]	<i>n</i> -pentane	-2.1160	-1617.3	0.0042
	<i>n</i> -hexane	1.6950	-2820.0	0.0153
	cyclohexane	0.5356	-2534.1	0.0149
	<i>n</i> -heptane	0.7757	-2693.8	0.0093
	<i>n</i> -octane	-0.7799	-2260.6	0.0102
	benzene	2.8474	-3360.9	0.0062
	toluene	3.1202	-3371.0	0.0104
	<i>o</i> -xylene	-1.7060	-1460.9	0.0106
	<i>m</i> -xylene	6.7903	-4047.7	0.0035
	<i>p</i> -xylene	-0.1242	-2085.8	0.0129
[OMIM][NO <sub>3</sub> ]	<i>n</i> -pentane	1.9711	-2573.1	0.0075
	<i>n</i> -hexane	3.0027	-2970.1	0.0167
	cyclohexane	2.4004	-2803.0	0.0120
	<i>n</i> -heptane	4.0424	-3533.4	0.0123
	<i>n</i> -octane	3.9761	-3505.5	0.0185
	benzene	1.8360	-2963.3	0.0040
	toluene	1.8365	-2903.0	0.0078
	<i>o</i> -xylene	-2.0829	-957.4	0.0027
	<i>m</i> -xylene	-1.2812	-1179.8	0.0056
	<i>p</i> -xylene	-1.5924	-1246.8	0.0066

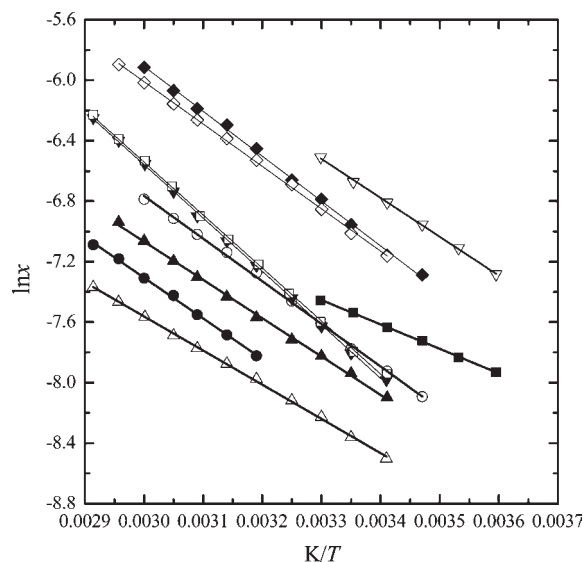
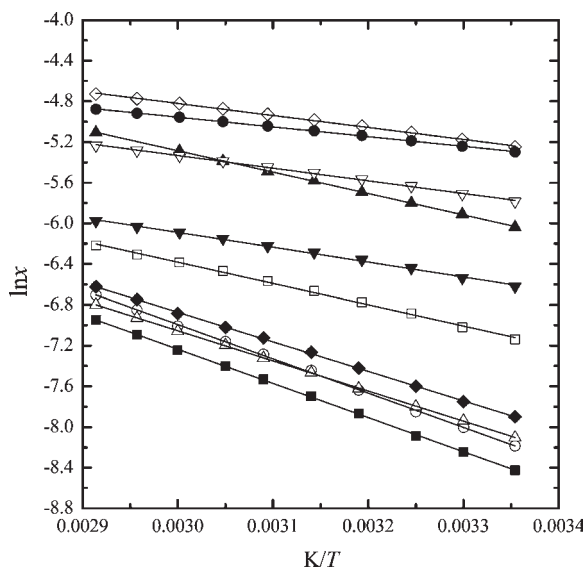


Figure 1. Mole fraction solubilities of two ILs in alkanes versus temperature: experimental data: ■, [HMIM][NO<sub>3</sub>] + *n*-pentane; ○, [HMIM][NO<sub>3</sub>] + *n*-hexane; ▲, [HMIM][NO<sub>3</sub>] + cyclohexane; ●, [HMIM][NO<sub>3</sub>] + *n*-heptane; △, [HMIM][NO<sub>3</sub>] + *n*-octane; ▽, [OMIM][NO<sub>3</sub>] + *n*-pentane; ◆, [OMIM][NO<sub>3</sub>] + *n*-hexane; ◇, [OMIM][NO<sub>3</sub>] + cyclohexane; ▼, [OMIM][NO<sub>3</sub>] + *n*-heptane; □, [OMIM][NO<sub>3</sub>] + *n*-octane; —, solubility curve calculated values according to eq 2.

polarity order. For the three xylene isomers, the order of solubility is: *m*-xylene > *o*-xylene > *p*-xylene, which is also related to their polarity order. In general, a relatively lower solubility of the two ILs in these solvents was observed. The alkyl chain increases in the cations of these ILs which can influence the



**Figure 2.** Mole fraction solubilities of two ILs in aromatic solvents versus temperature: experimental data: ■, [HMIM][NO<sub>3</sub>] + benzene; ○, [HMIM][NO<sub>3</sub>] + toluene; ▲, [HMIM][NO<sub>3</sub>] + *m*-xylene; □, [HMIM][NO<sub>3</sub>] + *p*-xylene; ▼, [HMIM][NO<sub>3</sub>] + *o*-xylene; △, [OMIM][NO<sub>3</sub>] + benzene; ◆, [OMIM][NO<sub>3</sub>] + toluene; ◇, [OMIM][NO<sub>3</sub>] + *m*-xylene; ▽, [OMIM][NO<sub>3</sub>] + *p*-xylene; ●, [OMIM][NO<sub>3</sub>] + *o*-xylene; —, solubility curve calculated values according to eq 2.

solubility as well. The solubilities of [OMIM][NO<sub>3</sub>] in alkanes are higher than that of [HMIM][NO<sub>3</sub>], which confirms the expectation from the theory of “similarity and intermiscibility”.

The ion–dipole type interaction between the solvent and the solute gets stronger with the increase of the polarity of the solvent, which can be explained as one of the reasons that these two ILs are partially soluble in the weak-polar solvents selected, whereas they are completely miscible with many strong polar solvents, such as water and alcohols (methanol, ethanol, etc.) as well as organic acids (formic acid, acetic acid, etc.).

In all cases, the calculated solubilities coincided with the experimental data, which verified the feasibility of correlating the solubility data of these two ILs in the 10 selected solvents by eq 2. Despite of their partial mole fraction solubility in the solvents investigated, the obtained solubility data would be useful for its purification. Also, the miscibility of these two ILs with many strong polar ones (water, alcohols, and organic acids) may have potential important implications in the design of separation processes.

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